

Simulating Flow of Nanofluids for Heat Transfer

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Abstract—A new class of fluids which is obtained by the dispersion of nanoparticles in base fluids, has been in focus due to its increased heat transfer characteristics. The usual dimension ranges from 10nm-50nm. The advantages of using nano particles over microparticles, in these suspensions are two fold. The particles being smaller, flow of nanofluids through pipes and channels cause lesser damage to the walls and the suspensions are more stable as the problem of sedimentation is drastically reduced. Designing light and compact heat exchangers is the ultimate aim in all the processes which involve generation and efficient removal of heat. In particular, in the electronics industry, miniaturization has resulted in the increase in the number of components per unit area. As a result there is an enormous generation of heat. Similarly in the automobile industry there is a requirement of efficient heat removal in the manufacturing processes and nanofluids therefore, can replace the conventional coolants both in the vehicles and in the industries like the tyre manufacturing sector where there is a continuous need for efficient heat removal. In this paper, we explore the characteristics of heat transfer for nanofluids enclosed within a cavity and study the phenomenon of natural convection for titanium dioxide nanoparticles dispersed in water. In particular we explore the effect of the volume fraction of the nanoparticles on the heat transfer rate of conduction and convection.

1. INTRODUCTION

Nanofluids, in the present decade has become a topic of extensive research due to the diverse applications. Engineering nanoparticles for efficient removal of heat has drawn a lot of attention ever since Choi[1] coined the term nanofluid which is a homogenous suspension of nanoparticles in a base fluid. In the present paper, we assume that the particles are distributed uniformly and there exists a thermodynamic equilibrium between the nanoparticles and the base fluid. We therefore assume the nanofluid as a single phase fluid with altered thermophysical properties. We investigate the heat transfer characteristics of TiO₂ nanoparticles dispersed in water[2]. The special application of this nanofluid is in solar collectors where this nanofluid enhances the heat transfer. This nanofluid is also used in the cosmetic and the paint industry and therefore exploring the transport properties like thermal conductivity and viscosity for this nanofluid is very significant. Earlier studies have been carried on CuO -water nanofluids in a differentially heated enclosure and the natural convection heat transfer has been explored[3].

2. DESCRIPTION OF THE PROBLEM

In the present paper we will study the natural convection in the TiO₂ nanofluid. Our system is similar to the conventional Rayleigh Benard system. It consists of two horizontal plates with the lower one at the higher temperature and the upper one at the lower temperature. These horizontal walls are maintained at constant temperatures. The side vertical walls are insulated and all the four walls of the cavity are impermeable and rigid. The cavity is filled with the TiO₂ nanofluid. We will focus on the buoyancy driven heat transfer using this nanofluid[4].

3. THERMOPHYSICAL PROPERTIES

$$\rho_{nf} = (1 - \phi)\rho_f + \phi\rho_s$$

$$\beta_{nf} = ((1 - \phi)\rho_f\beta_f + \phi\rho_s\beta_s)/\rho_{nf}$$

$$c_{nf} = ((1 - \phi)\rho_fc_f + \phi\rho_sc_s)/\rho_{nf}$$

$$k_{nf} = k_f(k_s + 2k_f - 2\phi(k_f - k_s))/(k_s + 2k_f + \phi(k_f - k_s))$$

$$\mu_{nf} = \mu_f(1 + 2.5\phi)$$

where the symbols have the following meaning.

ρ_{nf} represents the density of the nanofluid.

ϕ is the volume fraction of the nanoparticles suspended in base fluid

ρ_f is the density of the base fluid

ρ_s is the density of the nanoparticle.

μ_{nf} is the viscosity of the nanofluid

μ_f is the viscosity of the base fluid.

β_{nf} is the coefficient of volume expansion of the nanofluid

β_f is the coefficient of volume expansion of the base fluid

β_s is the coefficient of volume expansion of the nanoparticle

c_{nf} is the specific heat capacity of nanofluid at constant pressure

c_f is the specific heat capacity of base fluid at constant pressure

c_s is the specific heat capacity of nanoparticle at constant pressure

k_{nf} is the thermal conductivity of the nanofluid

k_f is the thermal conductivity of the base fluid

k_s is the thermal conductivity of the nanoparticle

[5],[6],[7],[8],[9].

4. HEAT TRANSFER CHARACTERISTICS

Our system is a bottom heated cavity filled with nanofluid . The basic objective is to study the effect of adding TiO_2 nanoparticles (to the base fluid) on the heat transfer rates of conduction and convection. Thermophysical properties of the nanofluids are temperature dependent[10]. In the present analysis, however, we consider only the density of the nanofluid to be temperature dependent and all other properties are approximated as constants over the temperature difference range under investigation.

The heat transfer characteristics are examined in terms of the Rayleigh numbers for the base fluid as well as the nanofluid.

We calculate the Rayleigh number for the given nanofluid using the formula from literature [11,12].

$$R_{nf} = \frac{(\rho\beta)_{nf} k_f (\rho c)_{nf} \mu_f R_f}{(\rho\beta)_f k_{nf} (\rho c)_f \mu_{nf}}$$

where R_{nf} and R_f represent the Rayleigh number of the nanofluid and the base fluid respectively. All symbols have been described in the previous section. The dependence of the Rayleigh number on the volume fraction is through the thermophysical properties which are all functions of the volume fraction.

5. RESULTS

We calculate the values of the thermal conductivity, viscosity, coefficient of volume expansion, density and the specific heat for the nanofluids for volume fractions ranging from 0.01-0.08 from the given relations. We compute the value of the Rayleigh number for the nanofluid for each volume fraction varying the Rayleigh number of the base fluid .

Table 1: Thermophysical Properties for TiO_2

$\rho_s(\text{kg/m}^3)$	$C_s(\text{J/kgK})$	$k_s(\text{W/mK})$	$\beta_s(\frac{1}{\text{K}})\times 10^6$
4250	686.2	8.95	9

Table 2

Vol.Fr	0	.01	.02	.04	.05	.06	.08
R_{nf}/R	1	.941	.8867	.7884	.7441	.7027	.62

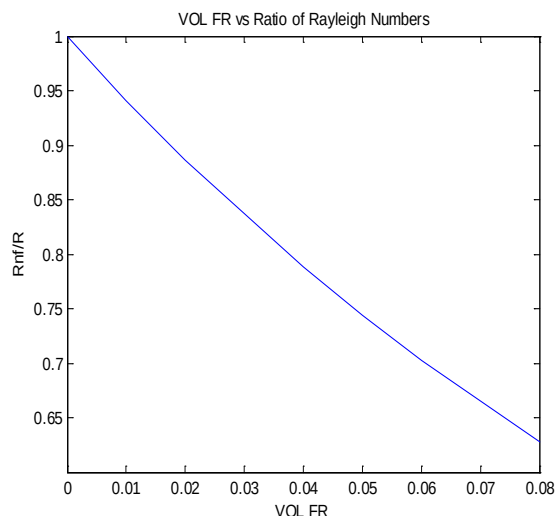


Fig. 1: R_{nf}/R as a function of vol. fr.

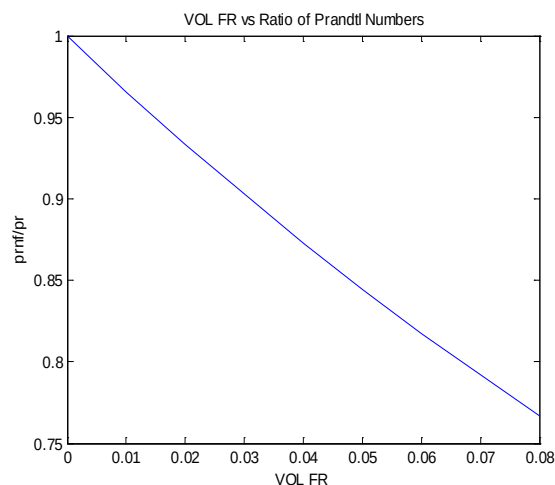


Fig. 2: Pr_{nf}/Pr as function of vol.Fr

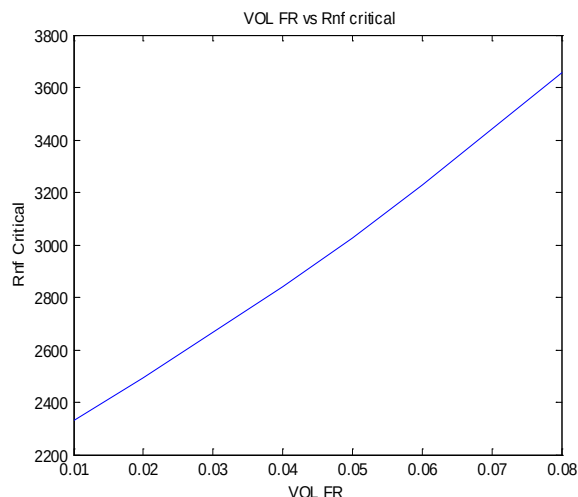


Fig. 3: R_{nf} critical as afunction of Vol. Fr

6. CONCLUSIONS AND DISCUSSIONS

From the calculations of the ratio of the Rayleigh number of the nanofluid to that of the base fluid, we find that it decreases with an increase in the volume fraction. This is evident from Fig.1. We have further calculated the ratio of the Prandtl number of the nanofluid to the Prandtl number of the base fluid and studied its dependence on volume fraction. The implication therefore is that addition of nanoparticles to the base fluid results in a decrease of the Rayleigh number of the nanofluid. Similarly addition of particles decreases the Prandtl number of the nanofluid. The critical Rayleigh number of the nanofluid at which convection sets in is illustrated in Fig. 3. Thus our conclusion is that the addition of nanoparticle has a stabilizing effect on the nanofluid. The transition to convection happens at higher values of the Rayleigh number in comparison to the base fluid. A further complexity can be introduced in the present problem where all the thermophysical properties will be a function of temperature. These results will be more accurate and free convection over larger temperatures can be investigated which will have industrial applications particularly in heat exchangers.

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